

# Design and test of a mass exchanger for oxygen control in liquid lead bismuth eutectic

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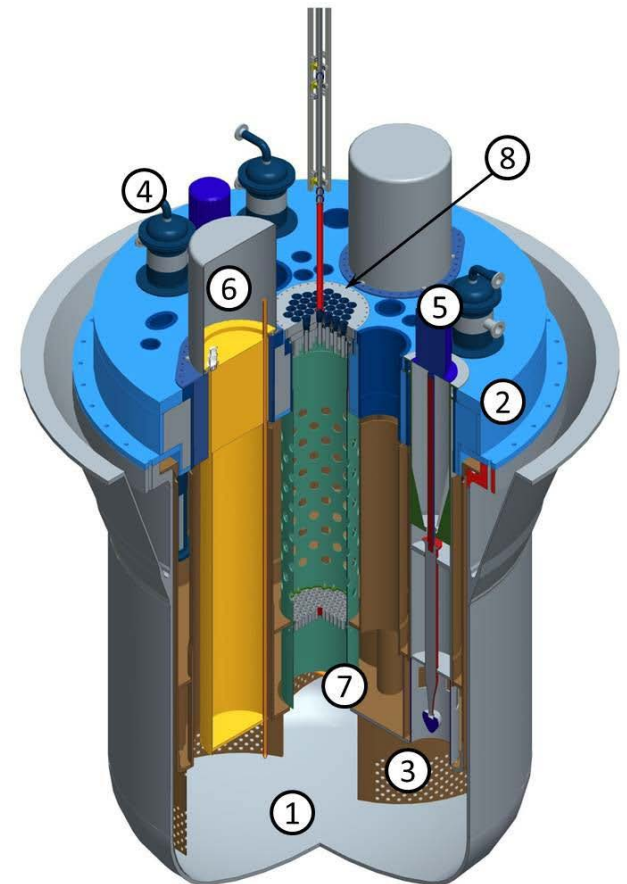
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- Introduction
  - MYRRHA
  - Issues and the importance of oxygen control in the use of LBE
  - Oxygen monitoring and control system
- PbO mass exchanger design
  - Overview
  - Test results in CRAFT loop
  - Modeling
  - Test results in MEXICO loop
- Conclusion

- **Lead-bismuth eutectic (LBE)** is the spallation target and primary coolant of MYRRHA:
- Opportunity
  - Excellent neutron yield
  - Low neutron reaction cross sections
  - Low melting point
  - High boiling point
  - Excellent thermal properties
- Challenge
  - Corrosive to steel
  - Liquid metal embrittlement

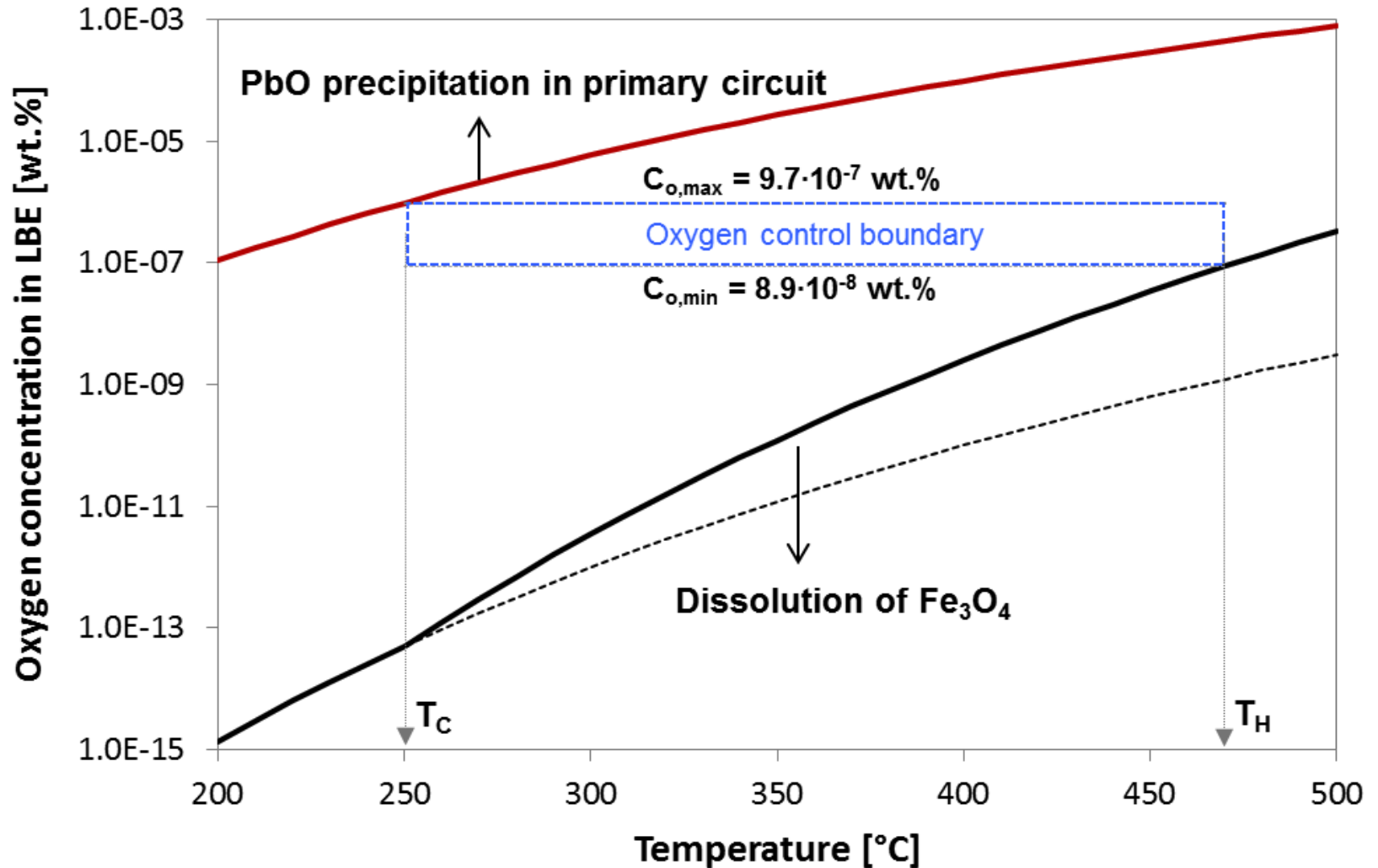


# Issues and the importance of oxygen control in the use of LBE

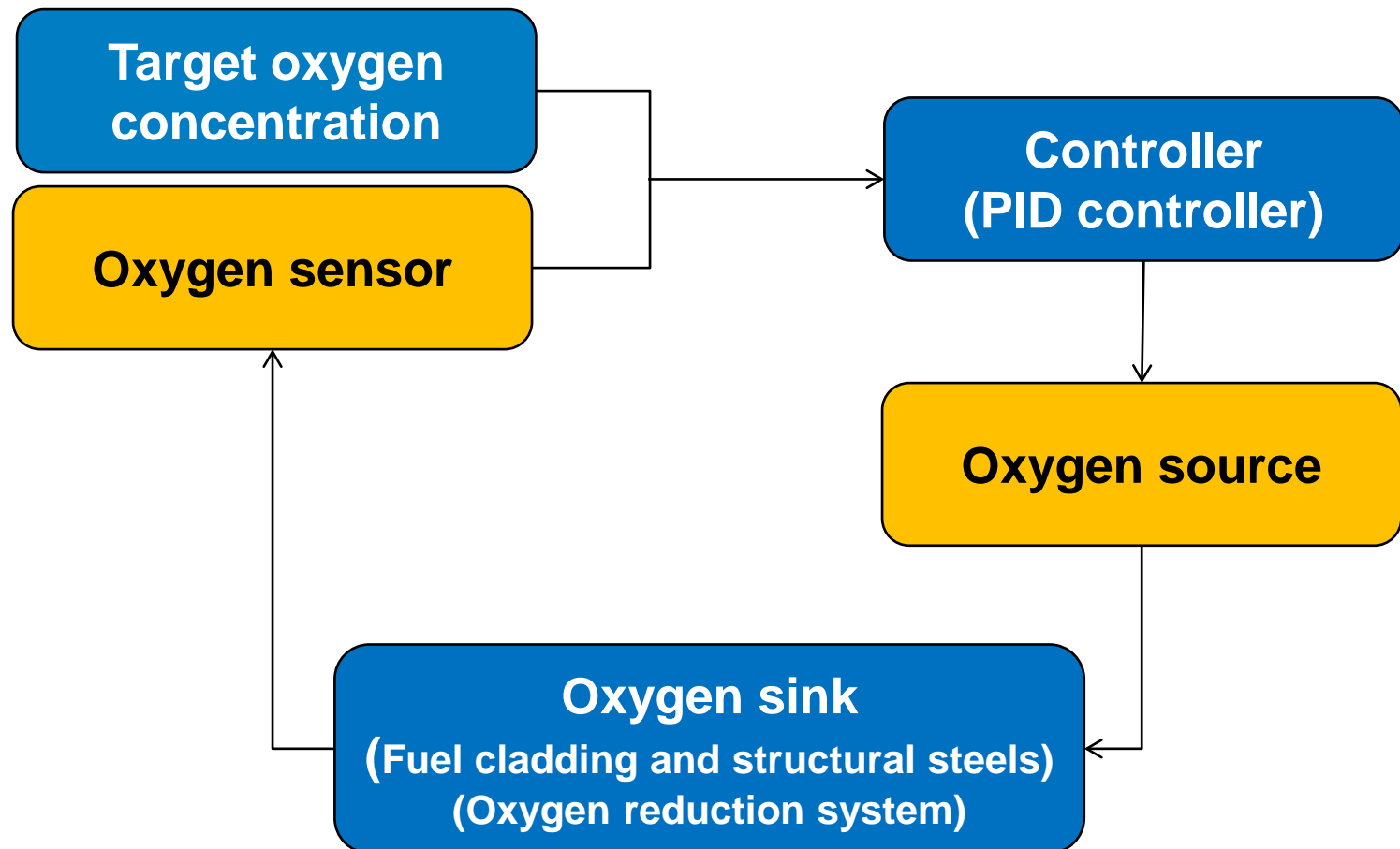
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- Material compatibility
  - Liquid metal corrosion
    - depends on material, temperature, flow rate, **oxygen**, etc
  - Liquid metal embrittlement
    - depends on material, temperature, **oxygen**, etc
- Risk of plugging
  - PbO formation
    - resulting from excessive **oxygen**
  - Corrosion products
    - depends on materials, temperature, flow rate, **oxygen**, etc

# Oxygen control boundary



# How to control dissolved oxygen in liquid LBE ?



# Oxygen control techniques

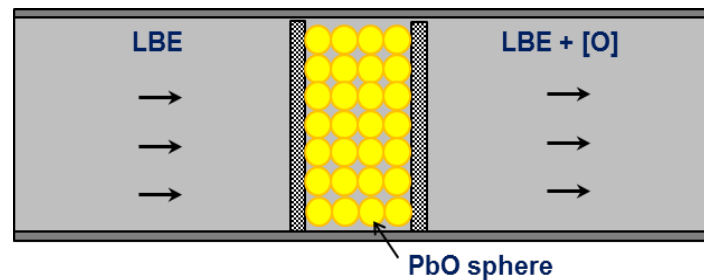
- Gas phase

- Pulse injection of oxygen with continuous gas injection
- Mixture gas  $H_2 / H_2O$  mixture

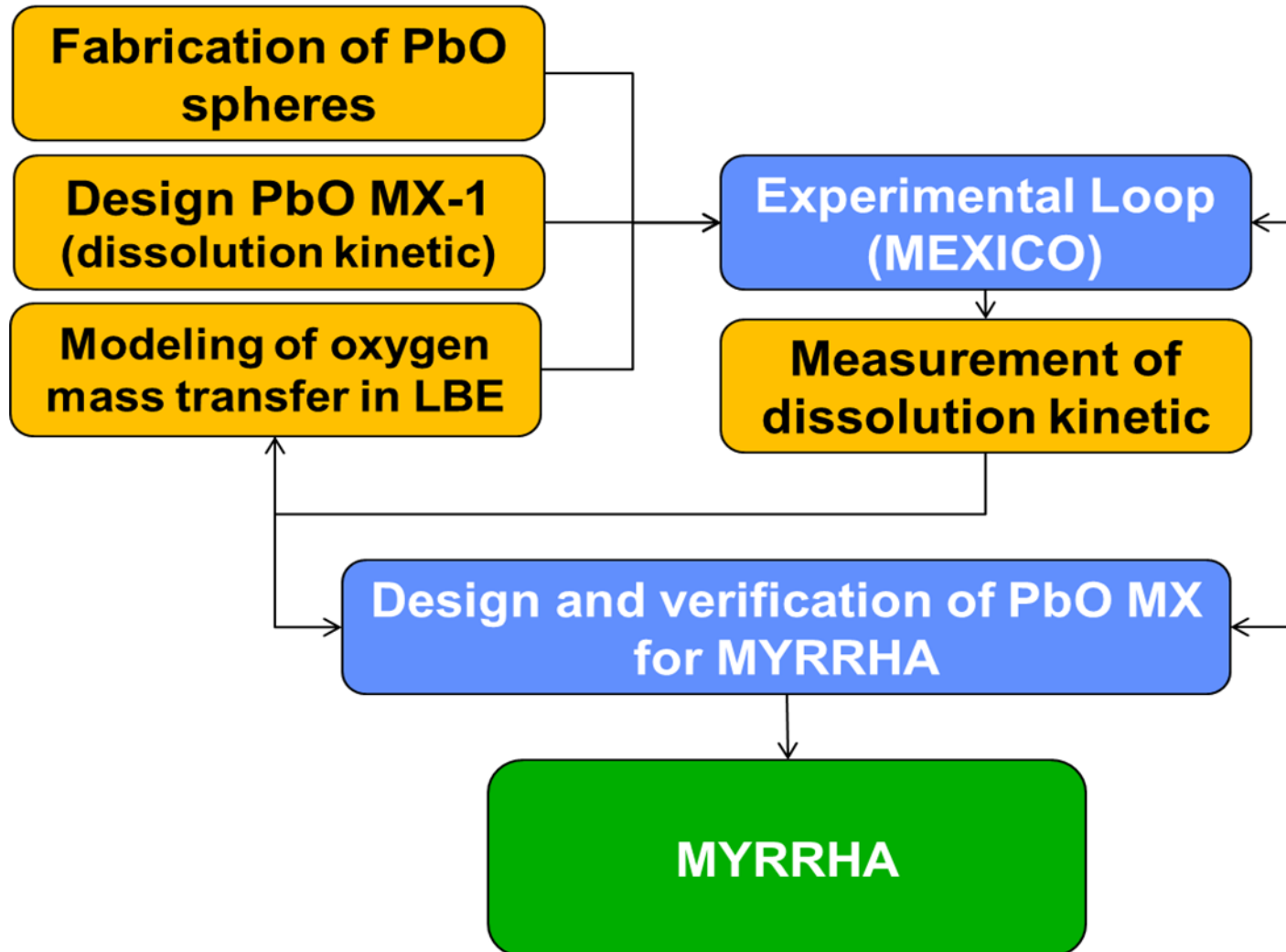
- Electrochemical method

- **Solid phase**

- Control dissolution rate of solid oxide (PbO)
- Solid PbO pebbles mass exchanger (PbO MX)

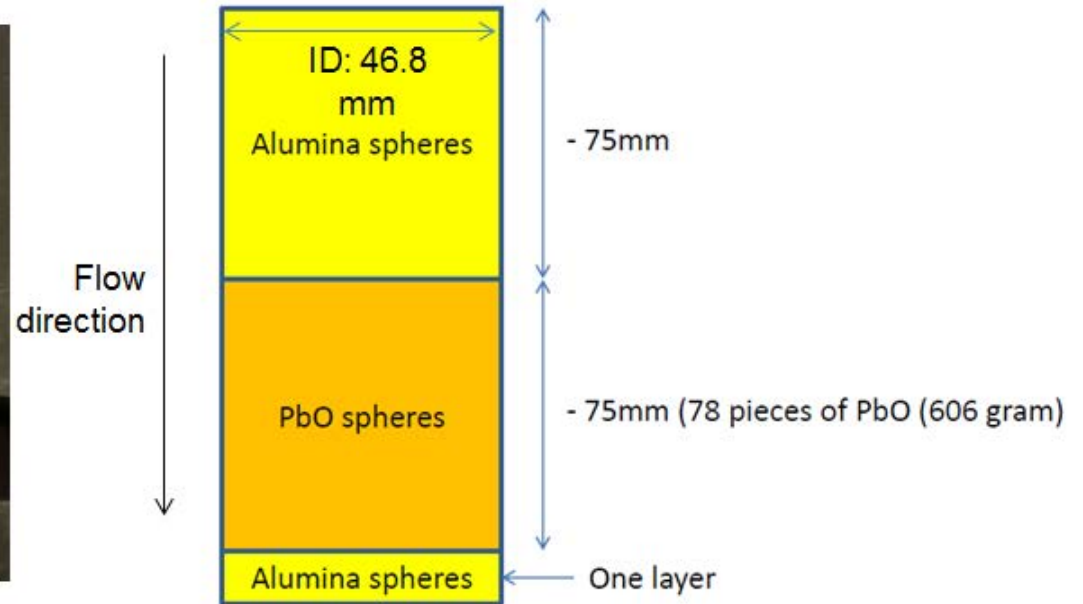


# PbO MX design: overview

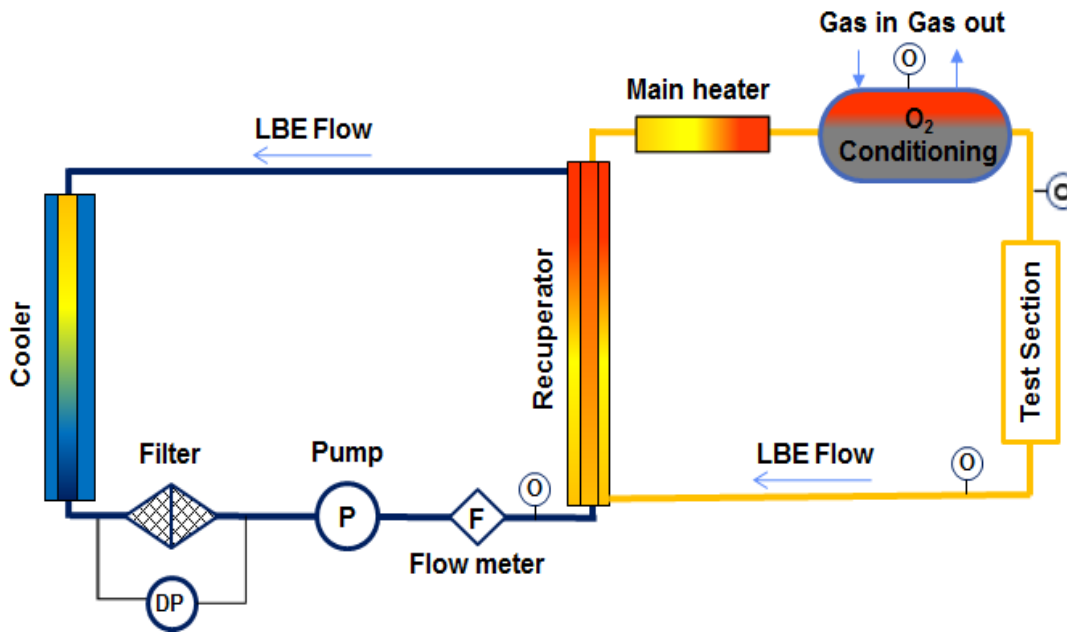




# PbO MX for CRAFT loop



# Experimental loop: CRAFT



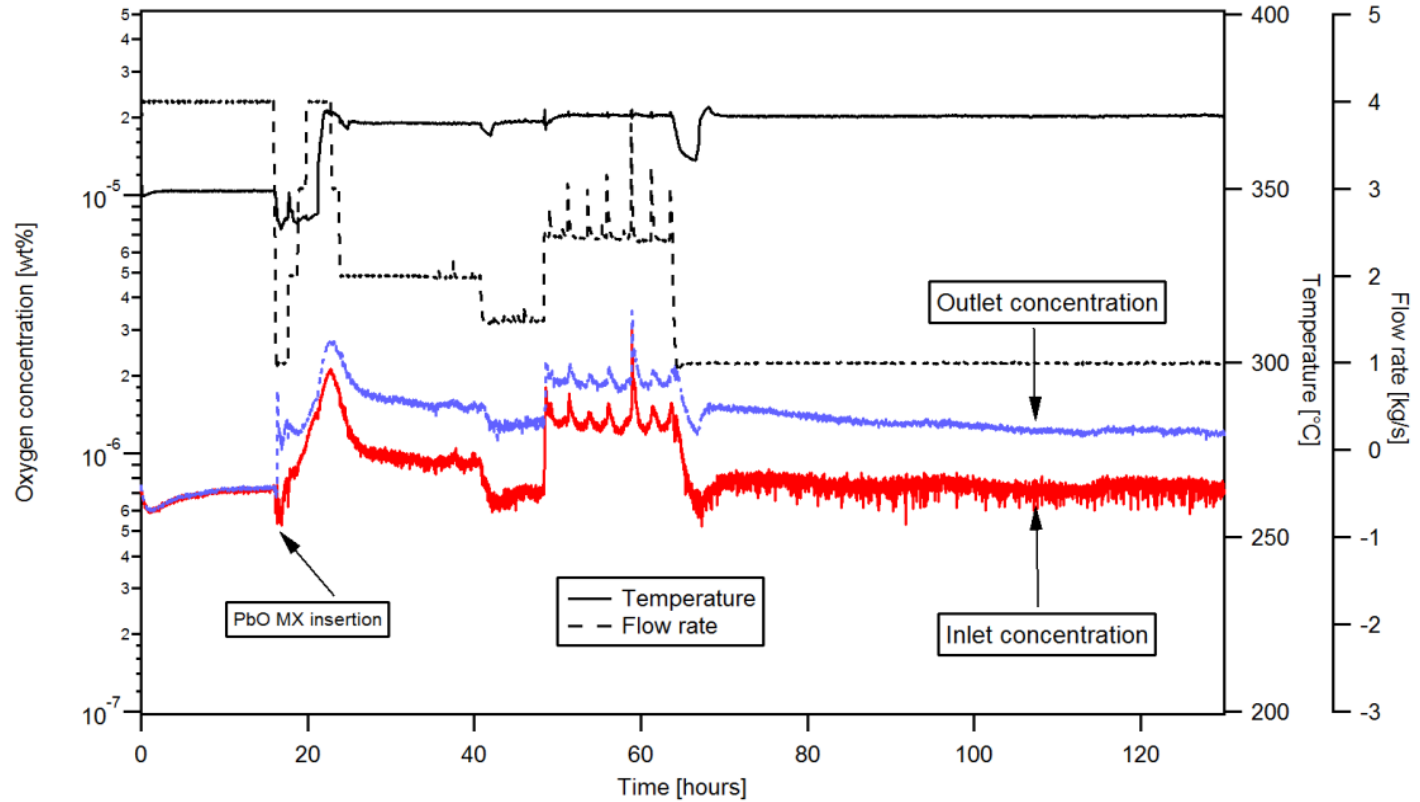
- Non-isothermal loop
- Oxygen conditioning system
- Wide range of operating conditions

## CRAFT



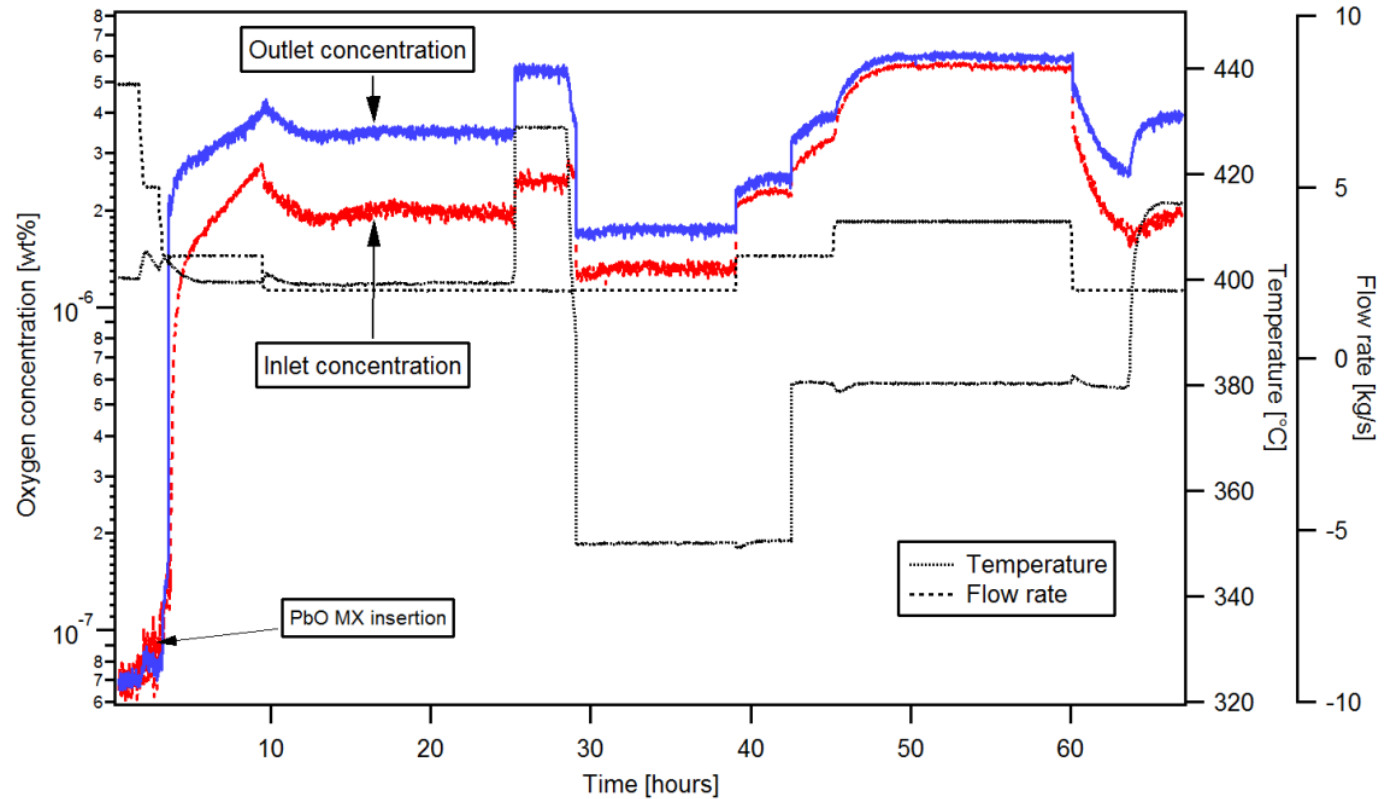
Corrosion in flowing LBE

# Dissolution rate measurements



- Fixed temperature
- Flow rate variation

# Dissolution rate measurements



- Temperature variation
- Flow rate variation

- Calculation of the **dissolution rate** of PbO packed bed of spheres from oxygen concentration measurements in CRAFT :

$$\dot{q} = \dot{m} \cdot (c_{out} - c_{in}) \quad [\text{g/h}] \quad (1)$$

- Calculation of **mass transfer coefficient for** each condition (temperature and velocity) :

$$\dot{q} = KA \cdot (c_s - c) \quad [\text{g/h}] \quad (2)$$

- $c_{out}$  = average outlet oxygen concentration,  $c_{in}$  = average inlet oxygen concentration,  $k$  = average mass transfer coefficient [g/cm<sup>2</sup>h],  $c$  = average oxygen concentration,  $A$  = surface area of PbO [cm<sup>2</sup>].

- Calculation of the **Sherwood number** from mass transfer coefficient :

$$Sh = K \cdot \frac{l}{D \cdot 360} \quad [-] \quad (3)$$

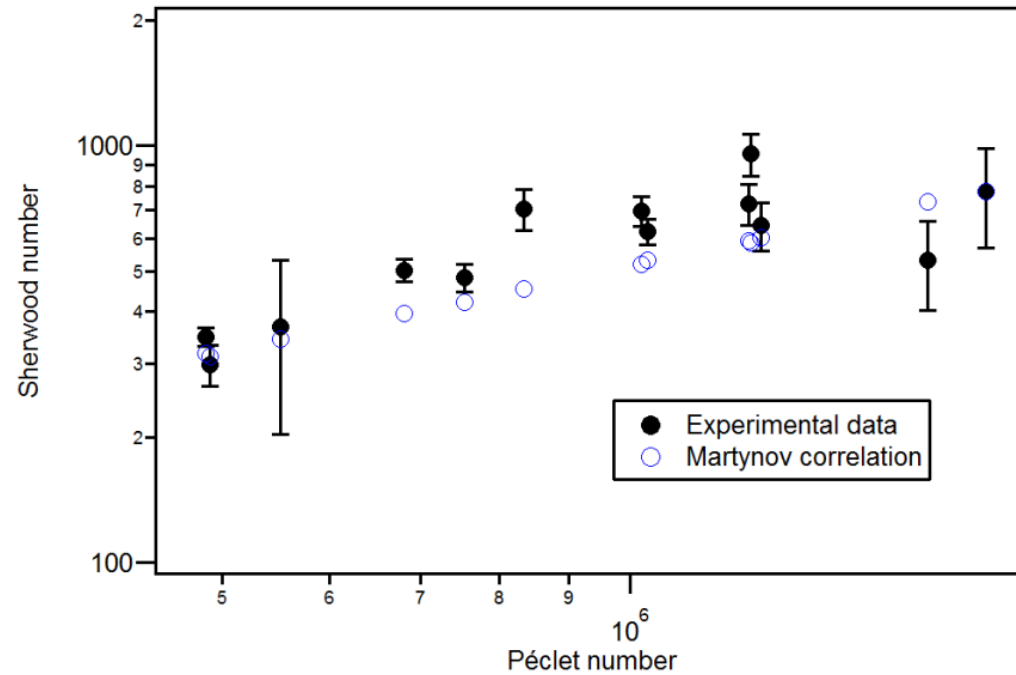
- Correlation of **Sherwood number** based on all measured data (temperature and velocity) :

$$Sh = A \cdot Re^n Sc^m \quad (4)$$

$$Sc = \frac{\nu}{D}, \quad Re = \frac{w \cdot l}{\nu} \quad l = \frac{2 \varepsilon \cdot d}{3(1 - \varepsilon)}$$

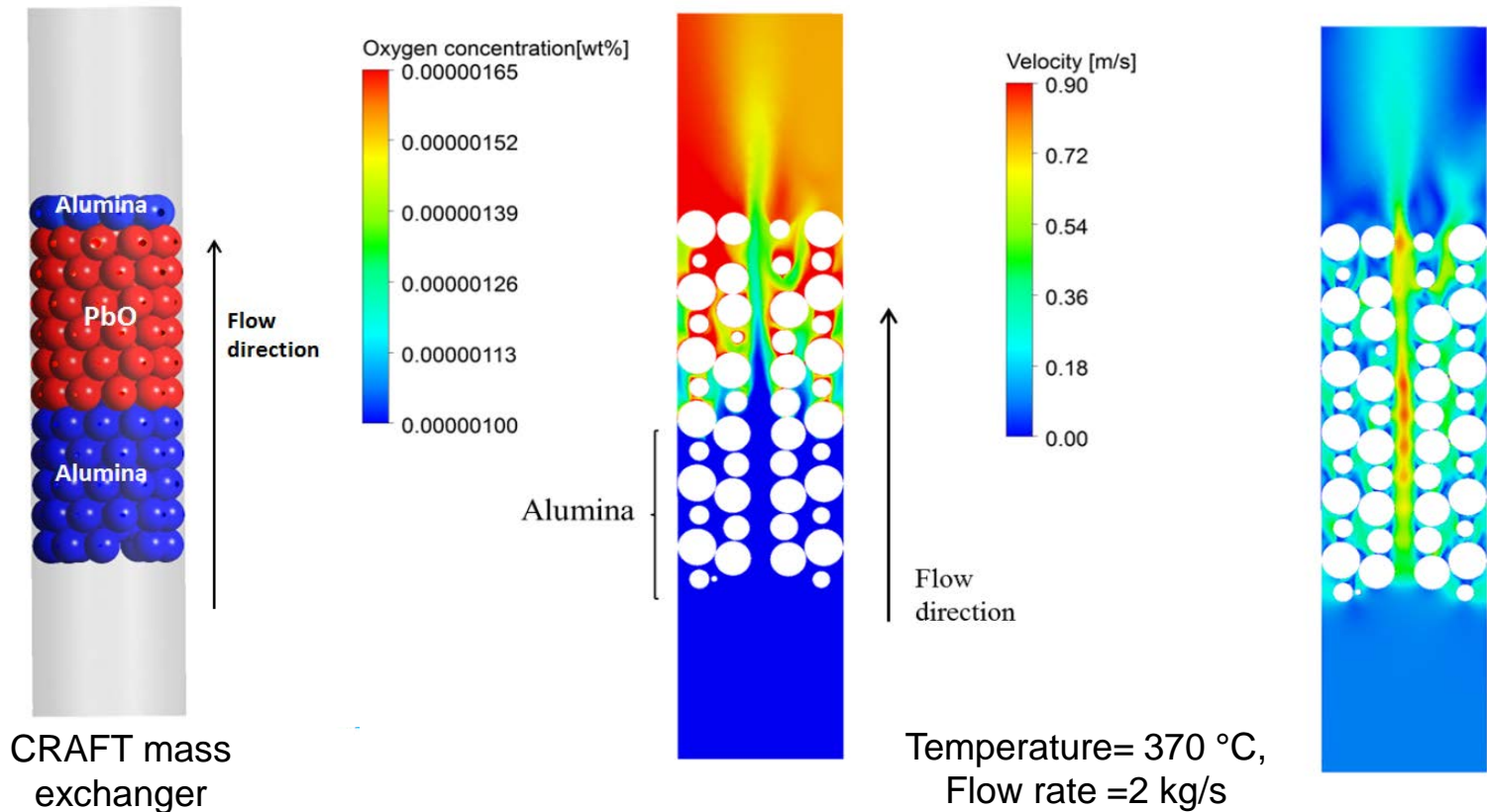
- Sh= Sherwood number, D=oxygen diffusion coefficient [m<sup>2</sup>/s], l=characteristic length [m],  $\nu$ = kinematic viscosity [m<sup>2</sup>/s], w = velocity [m/s],  $\varepsilon$  =porosity

# Experimental results



- Good agreement with Russian data
- Flat maximum at high velocity

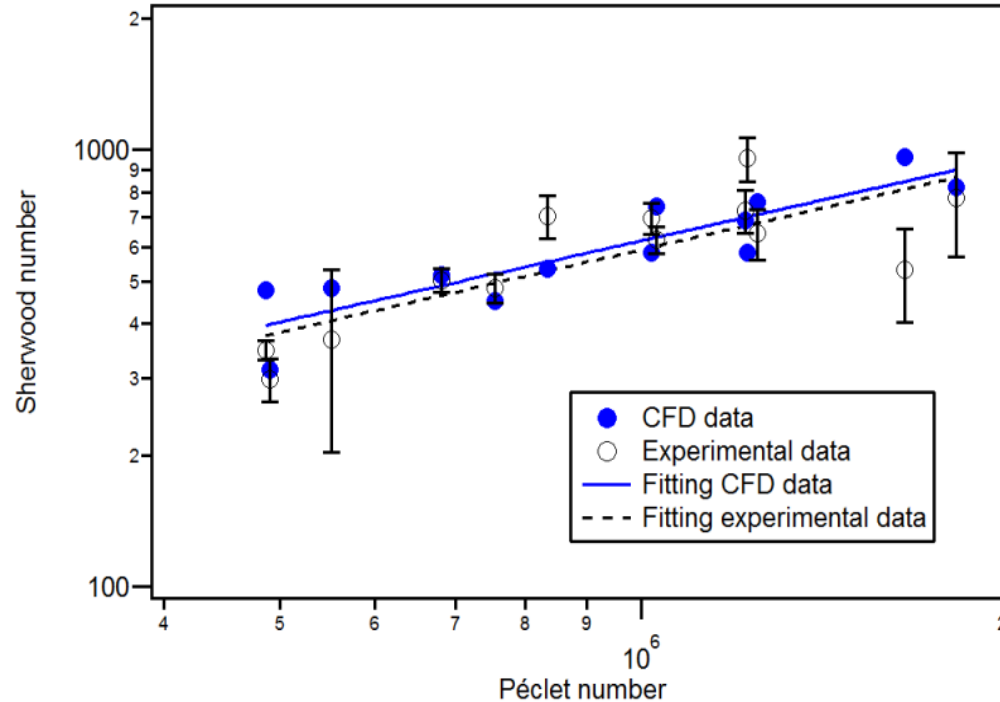
# Modeling: full scale simulation



- A. Marino, J. Lim, S. Keijers, J. Van den Bosch, J. Deconinck, "**Numerical modeling** of oxygen mass transfer from PbO spheres packed bed to liquid lead bismuth eutectic: A venturi-type PbO mass exchanger", Nuclear Engineering and Design, 265 (2013), 576–581
- A. Marino, J. Lim, S. Keijers, J. Van den Bosch, J. Deconinck, F. Rubio, K. Woloshun, M. Caro, S. A. Maloy, "Temperature dependence of **dissolution rate of a lead oxide** mass exchanger in lead-bismuth eutectic", Journal of Nuclear Materials, 450, (2014) 270-277
- A. Marino, J. Lim, S. Keijers, S. Vanmaercke, A. Aerts, K. Rosseel, J. Deconinck, J. Van den Bosch, "**A mass transfer correlation for packed bed of lead oxide spheres** in flowing lead-bismuth eutectic", International journal of heat and mass transfer, 80 (2015) 737-747



# Modeling validation

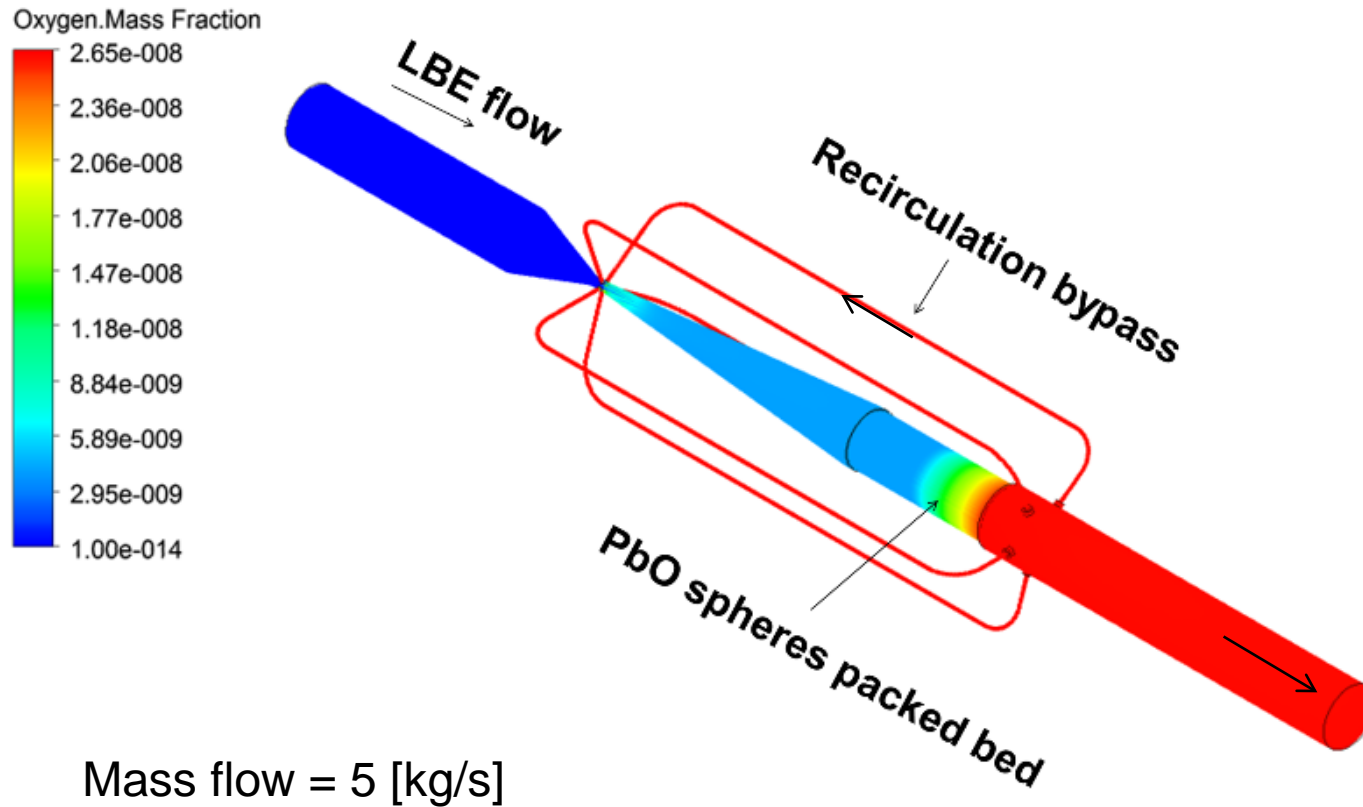


$$Sh = 0.07 \cdot Re^{0.87} Sc^{0.32}$$

**Preliminary  
correlation**

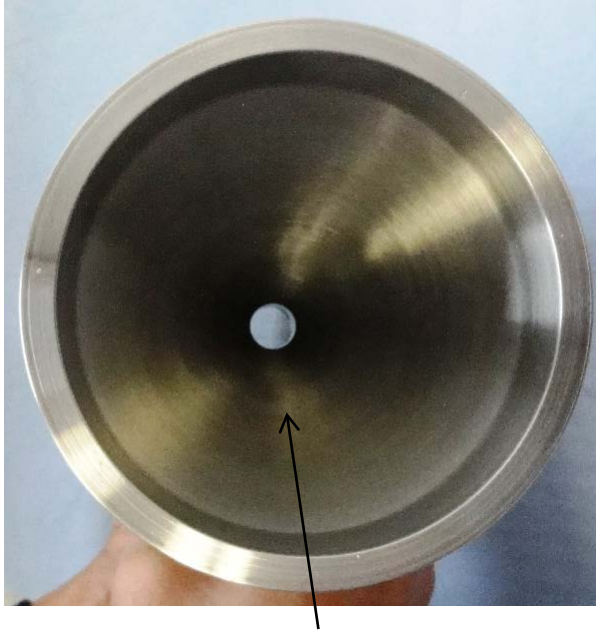
$$2000 < Re < 9000, 30 < Sc < 600$$

# Venturi-type mass exchanger



# Venturi-type mass exchanger

Venturi (top view)



- **Tungsten carbide (Hardide T) coating** on the inner surface of venturi neck to prevent erosion
- Pipe ID = 78 mm
- Venturi neck D = 12 mm

PbO basket (top view)

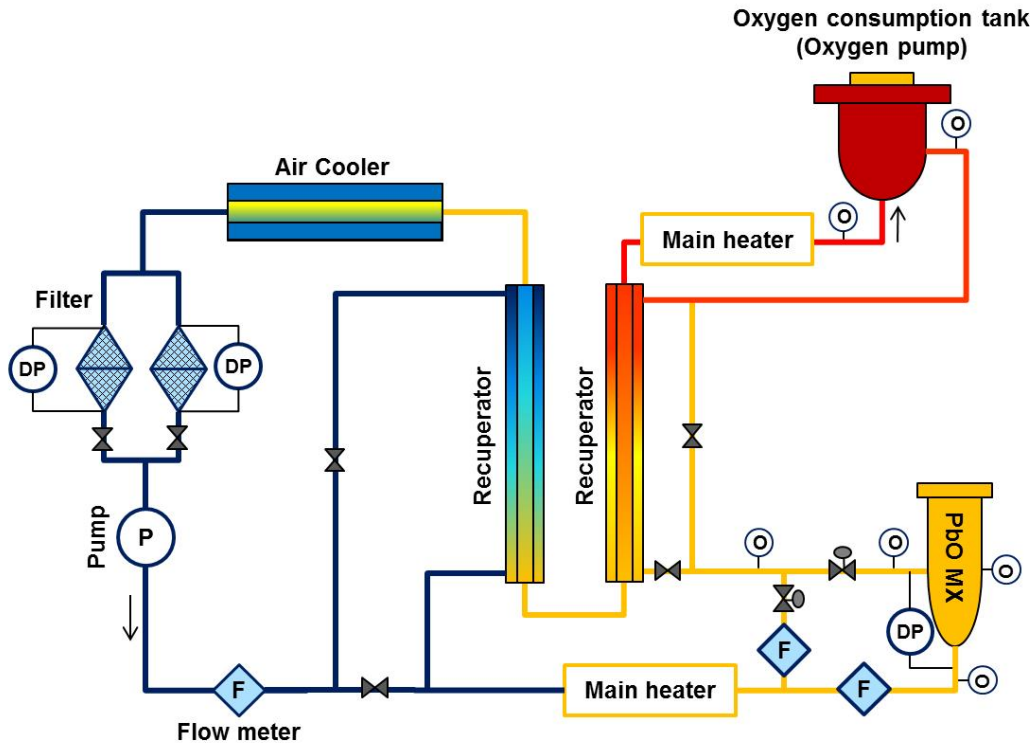


PbO sphere

: 12 mm diameter  
: 92.4% of theoretical density



# Experimental loop: MEXICO



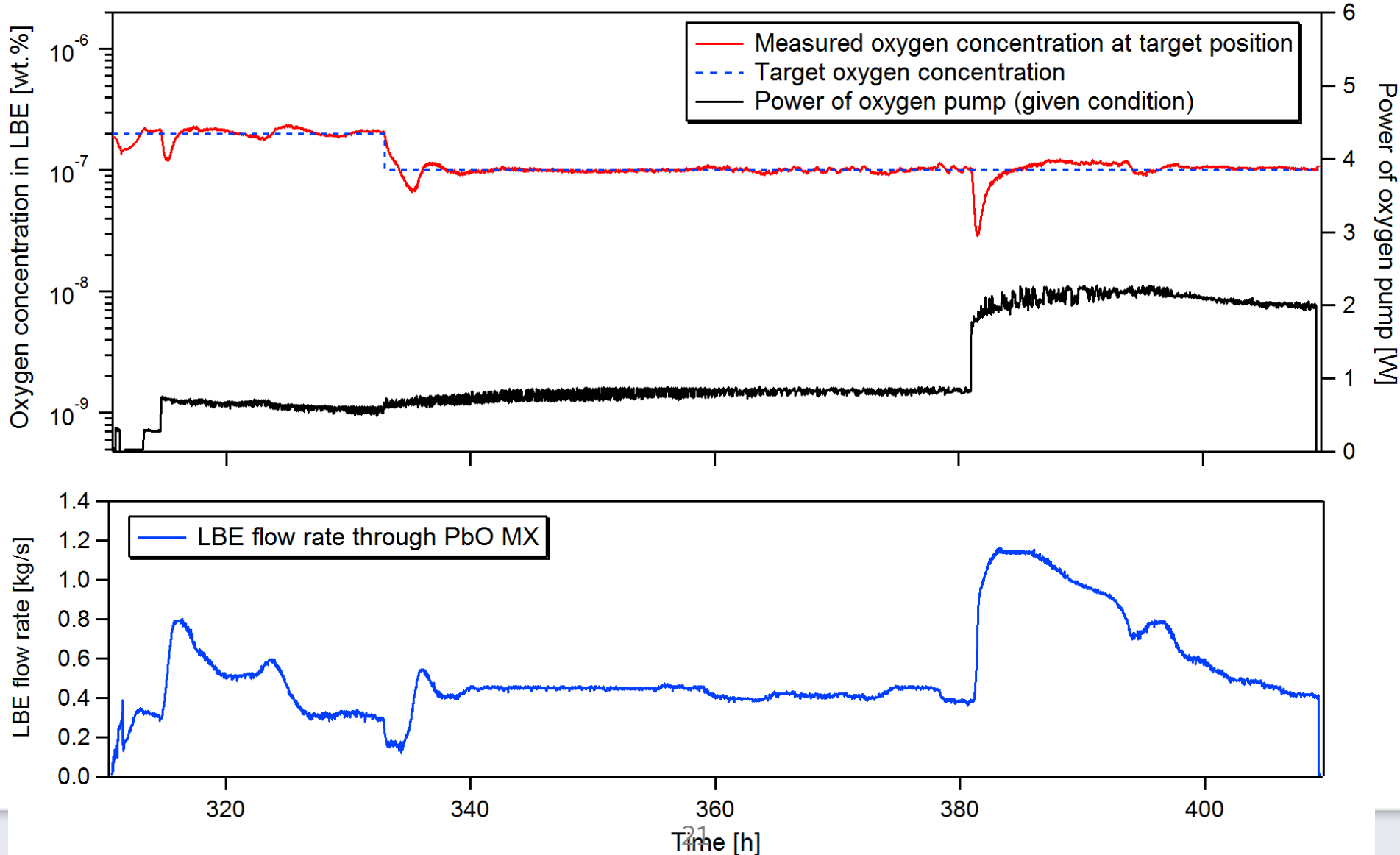
- Non-isothermal loop
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MEXICO



Integrated LBE chemistry

# Results : Oxygen control by PbO MX



Experiments on PbO MX dissolution have been successfully carried out at the CRAFT loop, SCK•CEN, Belgium:

- PbO spheres showed good mechanical and heat resistance
- Nearly-linear relation between velocity and dissolution rate: mass transfer limited kinetics
- No evidence of PbO poisoning
- Highly accurate oxygen control achieved by oxygen control systems during first experimental campaign.

Thank you for your attention!



## Results : PbO spheres after test



PbO particles might be cracked in the area of equator.